



## Structure and $\text{NO}_x$ storage behaviour of flame-made $\text{BaCO}_3$ and $\text{Pt}/\text{BaCO}_3$ nanoparticles

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### ABSTRACT

$\text{BaCO}_3$  and  $\text{Pt}/\text{BaCO}_3$  nanoparticles with high specific surface area (SSA) were prepared by flame spray pyrolysis (FSP). Their structure and behaviour during  $\text{NO}_x$  storage were investigated with special focus on the mechanistic and kinetic details. NO exposure of  $\text{BaCO}_3$  (BET:  $45 \text{ m}^2 \text{ g}^{-1}$ ) at various temperatures resulted in simple NO adducts. Low NO storage rate and  $\text{NO}_x$  storage capacity (NSC) were observed up to  $400^\circ\text{C}$ . In the presence as well as the absence of oxygen, NO was stored on  $\text{BaCO}_3$  showing the same IR-adsorption bands at  $100$ – $300^\circ\text{C}$ . Higher NSC and storage rates were observed for  $\text{NO}_2$  adsorption. DRIFT spectra showed that  $\text{NO}_2$  adsorption is accompanied by the formation of small amounts of NO which could be stored and subsequently oxidised again to  $\text{NO}_2$  adducts.

$\text{Pt}/\text{BaCO}_3$  prepared under identical conditions resulted in higher SSA ( $110 \text{ m}^2 \text{ g}^{-1}$ ) and showed increased NSC especially at higher temperatures. Enhanced DRIFT adsorption bands indicated the same NO adducts as obtained for the Pt-free  $\text{BaCO}_3$  during NO treatment. In the presence of oxygen and above the light-off temperature for NO oxidation, the consecutive reaction of stored nitrite to nitrate could be observed by in situ DRIFTS.  $\text{NO}_2$  adsorption led again to the highest NSC and storage rate. An optimal operation temperature window around  $300^\circ\text{C}$  was found where the  $\text{NO}_2$  storage rate was high and the catalysed competing  $\text{NO}_2$  conversion to NO was low enough to afford maximal NSC. Structural investigations indicate that only prolonged  $\text{NO}_x$  treatment leads to bulk barium nitrate: solid state conversion occurs after few hours. This supports the contention that the main contribution to  $\text{NO}_x$  storage during technical application in NSR catalysis occurs in the surface and subsurface regions of  $\text{BaCO}_3$ .

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### 1. Introduction

Global climate change is mainly caused by the increasing emission of carbon dioxide and other greenhouse gases. Finally, extreme  $\text{CO}_2$  emissions lead to drastic ecological, health and economic damages. Thus the reduction of all greenhouse gases is perhaps the largest looming public challenge we face today [1,2]. Legislative regulations can force e.g. the automotive industry to produce vehicles with low  $\text{CO}_2$  emissions. In this context diesel and lean burn engines are becoming more important. These engines possess intrinsic challenges with  $\text{NO}_x$  after-treatment in lean atmosphere. Beside selective catalytic reduction (SCR), another promising solution for passenger cars is the so-called  $\text{NO}_x$  storage reduction (NSR) catalyst or “Lean  $\text{NO}_x$  trap” (LNT) [3,4].  $\text{NO}_x$  is stored under fuel lean conditions and is reduced during short fuel

rich periods to harmless nitrogen. NSR catalysts consist of more than one component. Typically an alumina support carries ceria for oxygen and low temperature  $\text{NO}_x$  storage [5]. Additionally alkali metal oxides and alkaline earth metal oxides, especially  $\text{BaO}$  are needed for high temperature  $\text{NO}_x$  storage. Noble metals like Pt are used for the NO oxidation [6] during lean phases and for  $\text{NO}_x$  reduction during rich phases.

Several papers account for  $\text{NO}_x$  storage on  $\text{BaO}$  [7–9] or  $\text{BaO}$ -containing systems [10–13], but only some consider the presence of  $\text{CO}_2$  in the exhaust gas that reacts with  $\text{BaO}$  to  $\text{BaCO}_3$  [14–20]. The carbonate changes  $\text{NO}_x$  storage properties reducing the  $\text{NO}_x$  storage capacity (NSC). Studies of  $\text{NO}_x$  adsorption on  $\text{Pt}/\text{Ba}/\text{alumina}$  catalysts in which the barium component consists mainly of barium carbonate [15,21,22] show that  $\text{NO}_x$  reacting with surface barium sites forms barium nitrate which is much less thermally stable than bulk barium nitrate. These results emphasise the dependency of the storage behaviour on Ba loading and interfacial contact to the support. Nevertheless, to understand technical NSR catalysts and their storage behaviour under real working conditions in detail, it is

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also beneficial to elucidate  $\text{NO}_x$  and particularly NO adsorption on pure  $\text{BaCO}_3$  and Pt-loaded  $\text{BaCO}_3$ . A powerful technique to detect  $\text{NO}_x$  adsorbates in situ is diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS). The low surface areas of commercially available  $\text{BaCO}_3$  and resulting small intensities of the adsorption bands limit detection and interpretation of the DRIFTS spectra. For this reason, high SSA  $\text{BaCO}_3$  and Pt/ $\text{BaCO}_3$  were made by flame spray pyrolysis [23]. These nanopowders served as model systems for studying  $\text{NO}_2$  as well as NO adsorption on  $\text{BaCO}_3$ , the major storage component in NSR catalysts under real conditions.

## 2. Experimental

### 2.1. Commercial samples and preparation of high SSA powders

Commercially available  $\text{BaO}$  (Acros organics, 95% extra pure, granulate) and  $\text{BaCO}_3$  (Acros organics, 99.999%, extra pure) were compared with flame-made  $\text{BaCO}_3$  and Pt/ $\text{BaCO}_3$ . These materials were prepared using liquid barium 2-ethylhexanoate (30% in xylene, STREM chemicals) mixed in a 1:1 volume ratio with 2-ethylhexanoic acid (Riedel-de Haen, purum). For Pt/ $\text{BaCO}_3$  additionally platinum(II) acetylacetone (STREM, 98%) was added in order to get a Ba to Pt weight ratio of 20:1. The liquid precursor was then fed at  $3 \text{ mL min}^{-1}$  into the flame spray pyrolysis (FSP) reactor as described earlier [24] and dispersed with  $8 \text{ L min}^{-1}$   $\text{O}_2$  (PanGas, technical grade). The as-formed spray was ignited through a premixed pilot flame  $\text{O}_2/\text{CH}_4$  (PanGas, purity 2.5) in the ratio of 2:1.

### 2.2. Sample characterisation and transient $\text{NO}_x$ storage tests

IR spectra on powders were recorded in situ via DRIFTS. A FT-IR spectrometer (Bio-Rad, FTS 175 C) with a heatable reactor chamber [25], a 3D-praying mantis mirror system (Harrick) and a MCT detector were used. The resolution of the recorded spectra is  $4 \text{ cm}^{-1}$ . The catalyst powder was deposited in a quartz frit and placed in the reactor chamber. Gaseous components were fed into the reaction chamber and subsequently through the catalyst powder.

To obtain NSC values,  $\text{NO}_x$  breakthrough curves were measured using a quartz glass tubular reactor, surrounded with a heatable aluminium block. The gas outlet was analysed with a chemiluminescence detector (CLD-EcoPhysics 700 el ht).

The reaction gas mixtures for NO measurements consisted of 1000 (for DRIFTS experiments) or 100 (for NSC experiments) vol. ppm NO (Linde—2.5 vol.% NO purity 2.5 in Ar purity 5.0) balanced with nitrogen (Messer—purity 5.0) and optional with 10 vol.% oxygen (Messer—purity 3.5).  $\text{NO}_2$  adsorption experiments were performed with  $\text{NO}_2$  (Messer—1.51 vol.%  $\text{NO}_2$  purity 1.8, stabilised with 5.28 vol.%  $\text{O}_2$  purity 4.5) balanced with nitrogen to obtain the same concentrations as mentioned above. The gases were fed by mass flow controllers (Bronkhorst and Brooks) with a total flow rate of  $140 \text{ mL min}^{-1}$  ( $\text{SV} = 16\,000 \text{ h}^{-1}$ ).

Prior to the adsorption experiments, the samples were pre-treated with 30 vol.% oxygen (Westfalen—purity 3.5) in nitrogen at  $300^\circ\text{C}$  for 1 h. The adsorption temperature was subsequently set under nitrogen atmosphere.

$\text{NO}_x$  adsorption spectra were obtained by subtracting solid state spectra without  $\text{NO}_x$  from solid state spectra during  $\text{NO}_x$  treatment while the rest of the reaction conditions remained unchanged.

XRD patterns of the catalysts were measured on a STADI P (Stoe) diffractometer with a Cu-anode. The structure refinement according to the Rietveld method [26] was carried out with the software "FullProf" [27], integrated in the WinPLOTR software package.

For transmission electron microscopy (TEM) the powder samples were dispersed in ethanol and deposited onto a perforated

carbon foil supported on a copper grid (Okenshoji Co. Ltd.) performed on a CM30 (FEI; LaB6) operated at 300 kV.

## 3. Results and discussion

### 3.1. Structural studies

#### 3.1.1. Flame-made $\text{BaCO}_3$

Particles with SSA of  $45 \text{ m}^2 \text{ g}^{-1}$  were produced here. Fig. 1 shows "bean-like" shaped particles about 25 nm wide and 25–100 nm long, that are similar but smaller than reported in the literature [28]. Fig. 2 shows that they were orthorhombic  $\text{BaCO}_3$ , 5 h after synthesis, meaning that only little or no monoclinic  $\text{BaCO}_3$  was formed [28]. After calcination at  $400^\circ\text{C}$  in air for 1 h the SSA decreased by less than 10% to about  $41 \text{ m}^2 \text{ g}^{-1}$ .

#### 3.1.2. Flame-made Pt/ $\text{BaCO}_3$

The addition of Pt to  $\text{BaCO}_3$  resulted in a markedly higher SSA of  $110 \text{ m}^2 \text{ g}^{-1}$  which decreased to  $60 \text{ m}^2 \text{ g}^{-1}$  after calcination. In Fig. 3a the TEM of fresh FSP-made Pt/ $\text{BaCO}_3$  is shown. A fine, nanometre sized mesh-like structure of Pt/ $\text{BaCO}_3$  is responsible for the high SSA. The Pt clusters decrease the surface energy of the

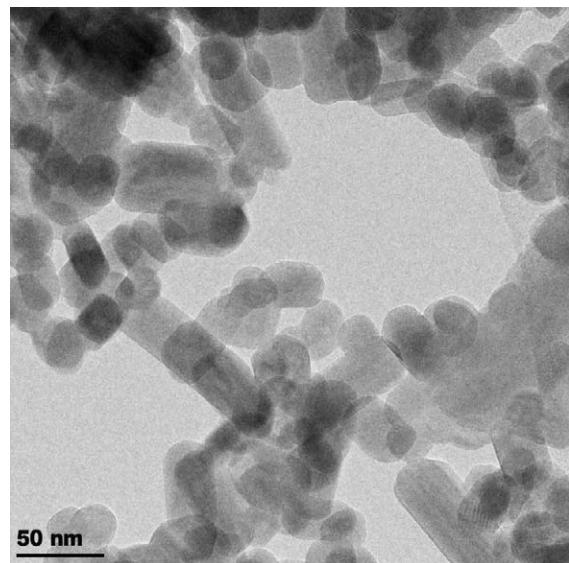


Fig. 1. TEM image of fresh flame-made  $\text{BaCO}_3$ .

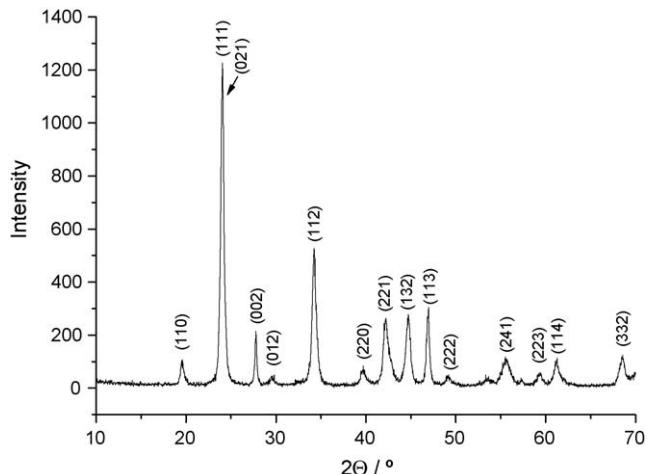


Fig. 2. XRD of the fresh flame-made  $\text{BaCO}_3$ .

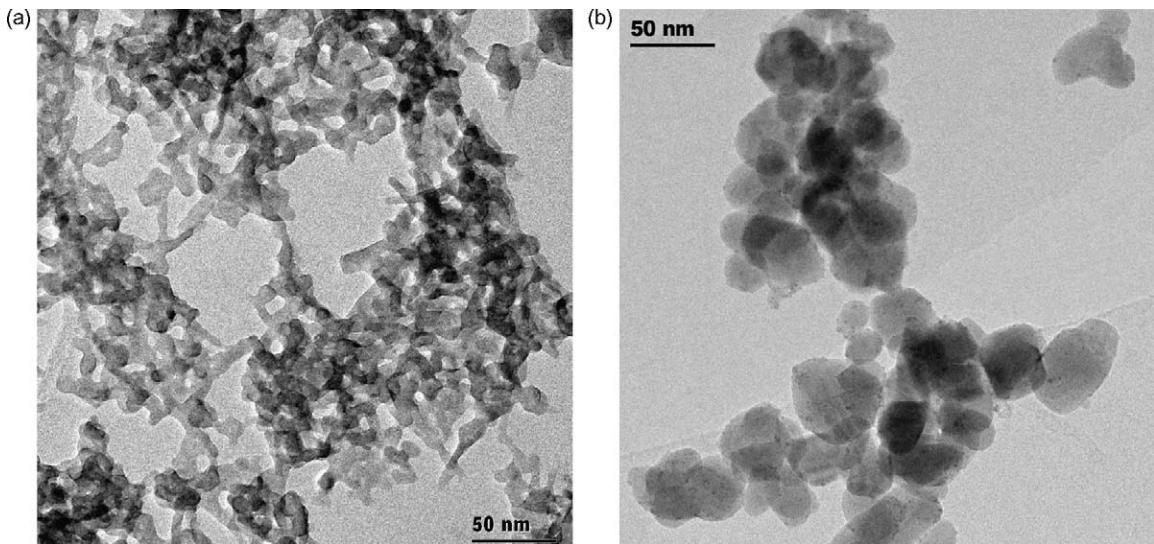


Fig. 3. TEM images (a) fresh Pt/BaCO<sub>3</sub> and (b) Pt/BaCO<sub>3</sub> pre-treated with N<sub>2</sub>/O<sub>2</sub> at 400 °C.

BaCO<sub>3</sub> crystallites hindering its surface growth (Zener pinning) during the short residence time in the flame [29]. When sintered at elevated temperatures (400 °C, 1 h) these structures changed into a spheroid shape as seen in Fig. 3b which resembled the pure BaCO<sub>3</sub> from Fig. 1. Fig. 4a shows the XRD pattern of freshly prepared powder indicating the presence of monoclinic BaCO<sub>3</sub> [30] which was stable for several days, probably due to the presence of Pt. After calcination in air at 400 °C, a phase change to the more stable orthorhombic BaCO<sub>3</sub> [31] was observed (Fig. 4b).

### 3.2. NO<sub>x</sub> adsorption on commercially available BaO and BaCO<sub>3</sub>

Fig. 5a shows the DRIFT spectra of BaO after 30 min of NO<sub>x</sub> treatment at 200 °C. Only a single band at 1246 cm<sup>-1</sup> with low intensity arises during NO treatment. This indicates that the surface is probably mainly covered by one type of species. In the presence of oxygen (10 vol.%) during NO adsorption, the intensity of the band at 1246 cm<sup>-1</sup> was increased while bands at 1376 and 1336 cm<sup>-1</sup> became discernible that are assigned to nitrates from NO<sub>2</sub> adsorption on BaO. The strongest band at 1246 cm<sup>-1</sup> which could be observed during NO adsorption was probably due to adsorbed NO. The NO formation may proceed via the well-discussed overall reaction [8,14,32,33]:



All three bands show different formation kinetics during NO<sub>2</sub> treatment and belong consequently to different species. The overall storage rate as well as the intensity of the bands increases during adsorption at 300 °C (see Fig. 5b). In addition to these bands, new ones at 1775 and 1500 cm<sup>-1</sup> were formed after 30 min NO<sub>2</sub> treatment. According to the solid state spectra of Ba(NO<sub>3</sub>)<sub>2</sub> (cf. Fig. 11a), these bands can be assigned to solid state nitrate bands. That means NO<sub>2</sub> adsorption occurred beside the solid state conversion which is fast enough at 300 °C. NO<sub>2</sub> adsorption at 100 °C led only to adsorption bands with an intensity of 0.2 (−lg R) after 30 min NO<sub>2</sub> treatment.

No bands were detectable during NO or NO/O<sub>2</sub> adsorption on commercial BaCO<sub>3</sub>. Only NO<sub>2</sub> treatment showed small gas phase bands of dosed NO<sub>2</sub> at 1600 and 1630 cm<sup>-1</sup> and formation of weak adsorption bands around 1350 cm<sup>-1</sup> (see Fig. 5a). These adsorption bands are located in the same region as the nitrate bands during

NO<sub>2</sub> adsorption on BaO. Thus NO<sub>2</sub> adsorption on BaCO<sub>3</sub> leads to the same species.

The NSC as well as the band intensities of NO<sub>2</sub> storage on BaCO<sub>3</sub> was much lower than on BaO which is, in this case, not attributable to the different SSA (BET<sub>BaO</sub>: 0.2 m<sup>2</sup> g<sup>-1</sup> and BET<sub>BaCO<sub>3</sub></sub>: 1 m<sup>2</sup> g<sup>-1</sup>). That means that the more active component for NO<sub>x</sub> storage is BaO but in catalysts under real working conditions the Ba component consists mainly of BaCO<sub>3</sub> [14]. To enable DRIFTS detection of adsorbates especially for NO treatment, BaCO<sub>3</sub> with higher BET surface was prepared by FSP.

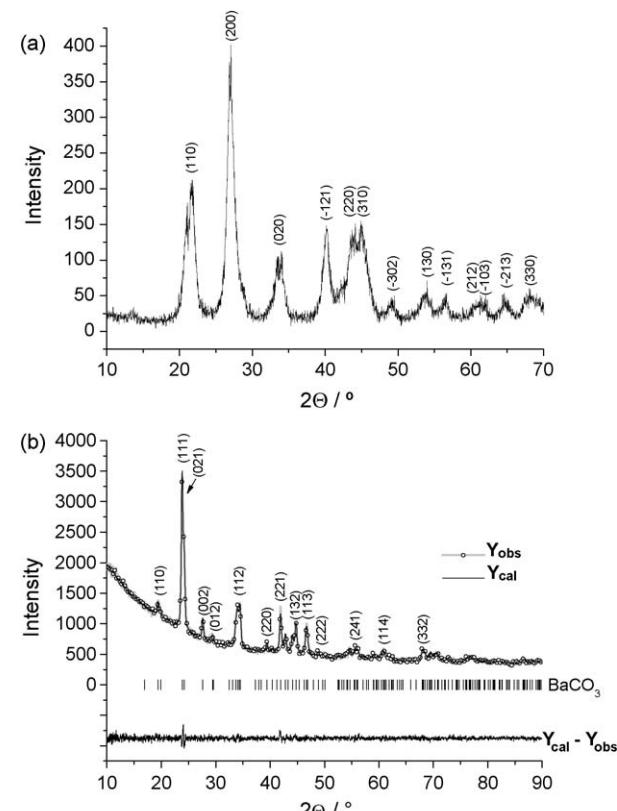


Fig. 4. XRD of (a) fresh Pt/BaCO<sub>3</sub> and (b) Pt/BaCO<sub>3</sub> pre-treated with N<sub>2</sub>/O<sub>2</sub> at 400 °C.

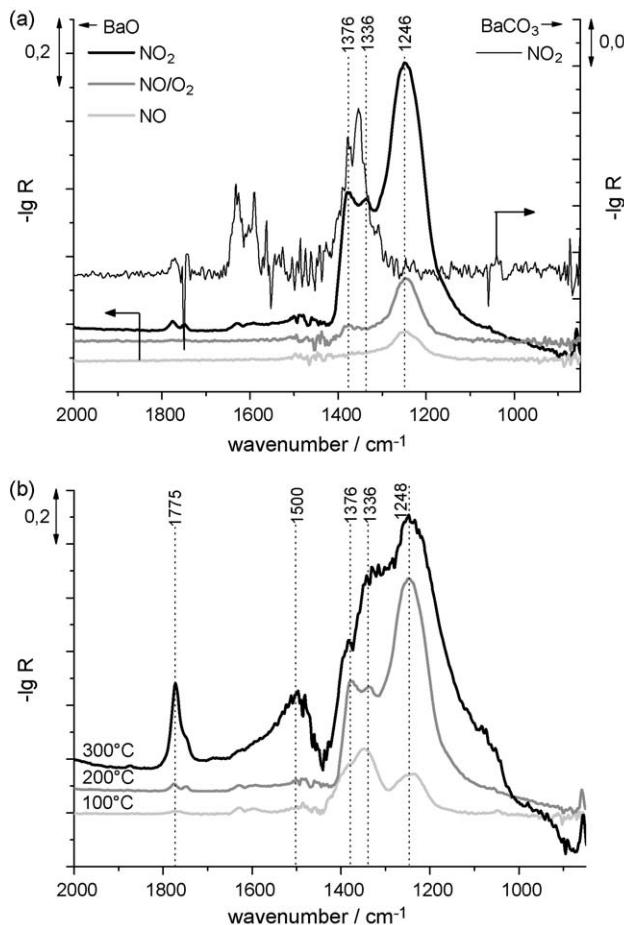


Fig. 5. (a) DRIFT spectra of NO, NO/O<sub>2</sub> and NO<sub>2</sub> adsorption on commercial BaO (left scale) and NO<sub>2</sub> adsorption on commercial BaCO<sub>3</sub> (right scale) at 200 °C after 30 min. (b) NO<sub>2</sub> adsorption on commercial BaO at 100, 200 and 300 °C.

### 3.3. NO<sub>x</sub> adsorption on high SSA BaCO<sub>3</sub>

High SSA BaCO<sub>3</sub> was prepared (untreated 45 m<sup>2</sup> g<sup>-1</sup> and after calcination 41 m<sup>2</sup> g<sup>-1</sup>) and on this material NO<sub>x</sub> adsorption led to detectable bands at 1300–1000 cm<sup>-1</sup> (Fig. 6). After 30 min of NO exposure, bands appeared at 1205 and 1080 cm<sup>-1</sup> with high intensities while the bands at 1035 and 1000 cm<sup>-1</sup> remained small which is in contrast to the later shown NO<sub>2</sub> adsorption. As neither

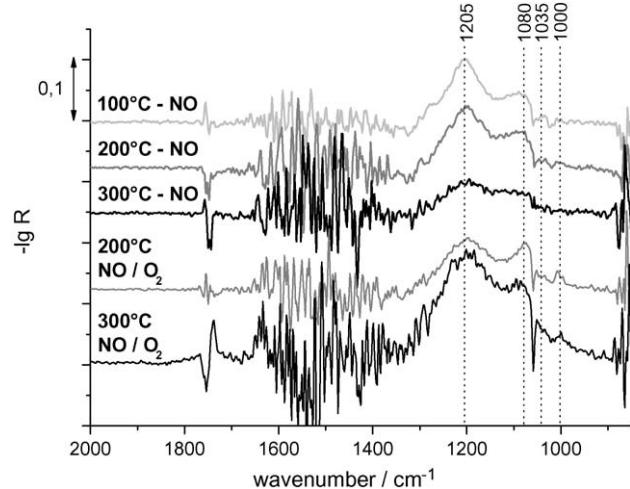


Fig. 6. NO<sub>x</sub> storage on flame-made BaCO<sub>3</sub> at different temperatures after 30 min.

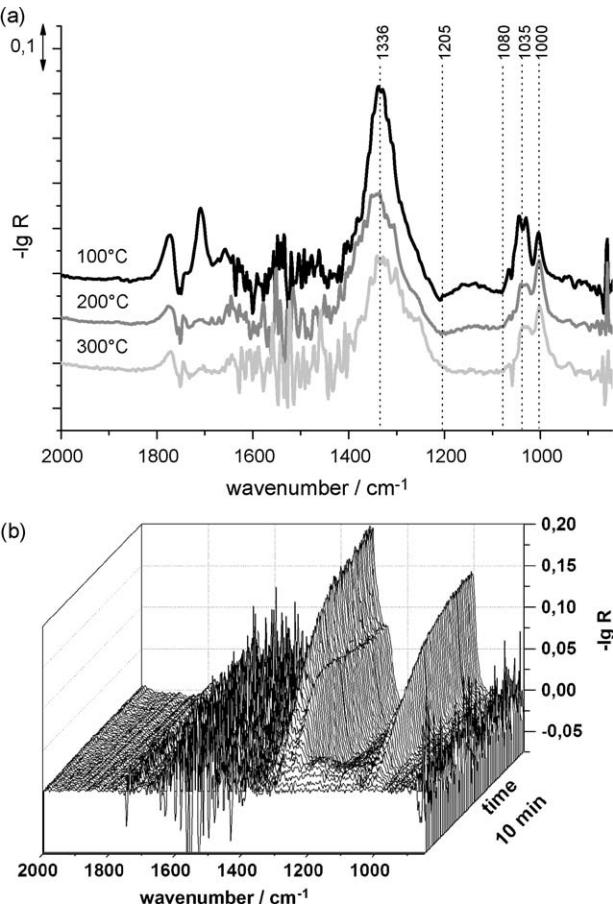
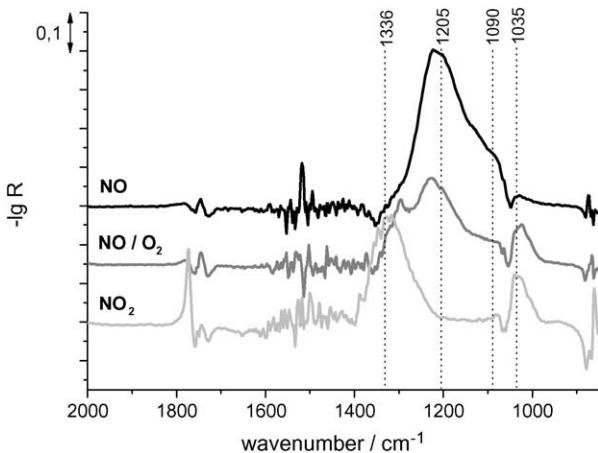


Fig. 7. (a) Temperature dependence of NO<sub>2</sub> storage on flame-made BaCO<sub>3</sub> after 30 min. (b) Development of DRIFT spectra during 10 min of NO<sub>2</sub> treatment of flame-made BaCO<sub>3</sub> at 200 °C.

molecular oxygen in the gas phase nor oxide anions in the lattice (there are only CO<sub>3</sub><sup>2-</sup> anions) were present, the formed species and their bands are attributed to simple NO adducts. Different adsorption geometries are conceivable to explain the variety of the obtained bands. Temperature variation from 100 to 300 °C showed no change in these bands, except at 300 °C where their intensities decreased marginally. The presence of oxygen during NO adsorption on BaCO<sub>3</sub> led to formation of the same bands that increased only marginally with higher temperatures. A bordered region of noise was detected from 1650 to 1400 cm<sup>-1</sup> and could only be observed in spectra of powder samples with high SSA. The origin of the noise remains unclear.

For NO<sub>2</sub> adsorption on BaCO<sub>3</sub> additional bands were obtained as seen in Fig. 7a. The strongest band is located at 1336 cm<sup>-1</sup> attributed to nitrates as observed during NO<sub>2</sub> treatment on BaO. In this context Schmitz and Baird [8] discuss the nomenclature of adsorbed species on BaO and define (NO<sub>2</sub><sup>-</sup>) as nitrite and (NO<sub>3</sub><sup>-</sup>) as nitrate species. Most discussed nitrates were formed from adsorbed NO<sub>2</sub> on lattice oxide ions. If we assume that BaCO<sub>3</sub> only consists of barium cations as well as carbonate anions (CO<sub>3</sub><sup>2-</sup>) (oxide anions, O<sup>2-</sup>, should be absent) and NO<sub>x</sub> adsorbed on carbonate sites, the discussion concerning nitrite and nitrate species would become difficult. To simplify, we assume the presence of oxide on the barium carbonate surface by decarbonation during NO<sub>x</sub> treatment [14]. Then adsorbed NO<sub>2</sub> leads naturally to nitrate bands and NO adsorption on the surface results in nitrite formation. Furthermore the bands at 1035 and 1000 cm<sup>-1</sup> were intensified during NO<sub>2</sub> treatment. Variation of the temperature at 100–300 °C led only to changes in the intensity of the obtained bands.



**Fig. 8.** Influence of gas composition during adsorption on Pt/BaCO<sub>3</sub> at 200 °C after 30 min.

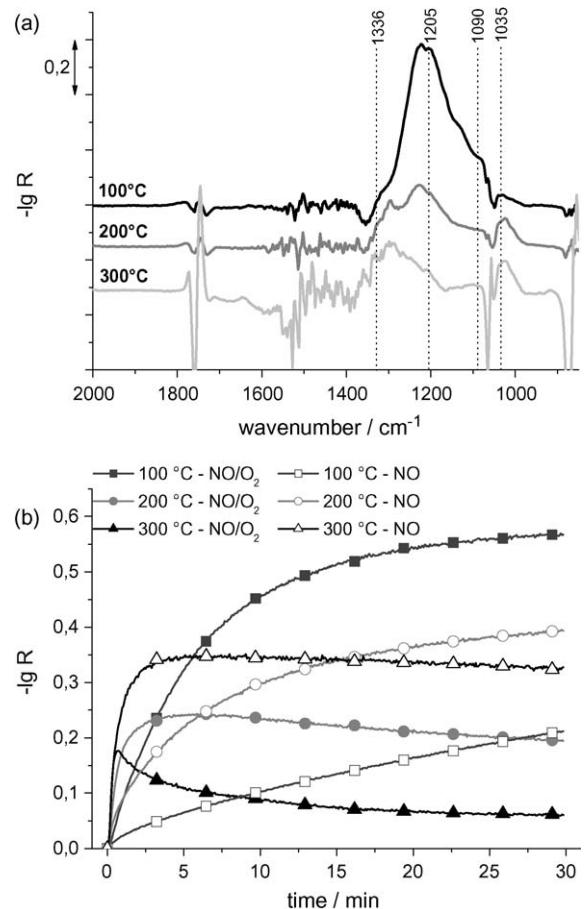
Regarding the kinetics of the band at 1205 cm<sup>-1</sup>, a maximum intensity could be observed initially during NO<sub>2</sub> adsorption. This is shown in Fig. 7b for NO<sub>2</sub> adsorption at 200 °C with the maximum intensity after 1 min. The band of the intermediate species represents the vibration mode of a nitrite as seen in Fig. 6. NO might be formed during NO<sub>2</sub> treatment according to Eq. (1) [14] and after its adsorption on BaCO<sub>3</sub>, gaseous NO<sub>2</sub> oxidises it.

#### 3.4. Influence of platinum: NO<sub>x</sub> adsorption on Pt/BaCO<sub>3</sub>

Adsorption measurements of NO, NO/O<sub>2</sub> and NO<sub>2</sub> were performed on Pt/BaCO<sub>3</sub> (Fig. 8). To single out the effect of Pt during NO<sub>x</sub> storage, the same reaction conditions were applied noting, however, that the sample SSA was 110 m<sup>2</sup> g<sup>-1</sup> before pre-treatment and 60 m<sup>2</sup> g<sup>-1</sup> before NO<sub>x</sub> adsorption. Adsorption of NO at 200 °C led qualitatively to the same nitrite bands as obtained during NO treatment on BaCO<sub>3</sub>. Comparing these band intensities during NO adsorption on Pt/BaCO<sub>3</sub> were significantly enhanced (Figs. 6 and 8). This was probably caused by the higher SSA of Pt/BaCO<sub>3</sub> than BaCO<sub>3</sub> (BET: 41 m<sup>2</sup> g<sup>-1</sup>). Note that the higher intensity of the observed nitrites and nitrates after exposure to NO somehow stands in contrast to similar studies performed on conventional Pt/Ba/alumina catalysts, where higher intensities are observed after exposure to NO<sub>2</sub> [13]. The reason for this behaviour is not clear yet but may be tentatively attributed to the different material (BaCO<sub>3</sub>) and the fact that different adsorbed species might have altered extinction coefficients.

In the presence of oxygen at 200 °C the nitrite bands at 1205 and 1090 cm<sup>-1</sup> exhibited a maximum after 5 min and new bands (1336 and 1035 cm<sup>-1</sup>) were formed (the spectrum after 30 min NO/O<sub>2</sub> storage is shown in the middle of Fig. 8). These new bands were already observed during NO<sub>2</sub> adsorption on BaCO<sub>3</sub> and could be assigned to nitrate. This means that nitrite species were oxidised to nitrate during NO/O<sub>2</sub> storage. This oxidation was not observed during NO/O<sub>2</sub> storage on BaCO<sub>3</sub>, and therefore the effect can be ascribed to Pt which is a well-known catalyst for NO oxidation. The onset of this reaction depends on the support, Pt dispersion [34] as well as the feed composition [6,35]. Typically NO oxidation starts at 100–200 °C. Thus it is reasonable to assume that formed NO<sub>2</sub> acts as oxidant and reacts with the adsorbed nitrites to nitrates. Additionally the direct storage of in situ formed NO<sub>2</sub> is possible.

The observed consecutive reaction showed strong temperature dependence (see Fig. 9a). NO/O<sub>2</sub> adsorption at 100 °C led to the same adsorption bands as NO adsorption without oxygen. Only the



**Fig. 9.** (a) Temperature dependence of NO/O<sub>2</sub> storage on Pt/BaCO<sub>3</sub> after 30 min. (b) Development of the nitrite band at 1205 cm<sup>-1</sup> during NO/O<sub>2</sub> and NO storage on Pt/BaCO<sub>3</sub>.

band intensities were increased in the presence of oxygen but the oxidation reaction was too slow or did not take place. At 200 °C the oxidation of stored NO was fast enough to be observed via DRIFTS. Fig. 9b shows the kinetics of the nitrite bands at 1205 cm<sup>-1</sup> for different temperatures, with and without oxygen. Increasing the storage temperature to 300 °C led to a faster consecutive reaction. The spectrum after 30 min NO/O<sub>2</sub> treatment is similar to the spectrum resulting from NO<sub>2</sub> treatment of Pt/BaCO<sub>3</sub> or BaCO<sub>3</sub>. They all show nitrate bands in the regions of 1336 and 1035 cm<sup>-1</sup> and negligible nitrite bands.

#### 3.5. NSC and the influence of NO/O<sub>2</sub>–NO<sub>2</sub> equilibrium

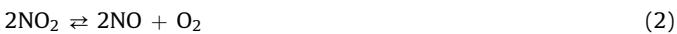
The NO<sub>x</sub> storage capacity of BaCO<sub>3</sub> and Pt/BaCO<sub>3</sub> was obtained by the evaluation of breakthrough curves, measured using a tubular reactor. NO<sub>x</sub> saturation of the catalyst was assumed when the NO<sub>x</sub> outlet concentration was equal to the NO<sub>x</sub> inlet concentration. Due to the signal to noise ratio of the used analyser, very slow NO<sub>x</sub> storage rates led probably to an underestimation of the NSC values, however, for technical applications these slow storage rates are anyhow not interesting. The time needed for NO<sub>x</sub> saturation depends on the kinetic and is a function of temperature, feed composition and the chemical composition of the sample. Table 1 shows higher NSC with increasing temperature (here: 100 °C compared to 400 °C). The NSC for treatment with NO<sub>2</sub> is higher than for NO/O<sub>2</sub> which in turn is higher than for pure NO. The influence of Pt during NO/O<sub>2</sub> treatment especially for higher temperatures enhanced the NSC according to the DRIFTS investigations (cf. Figs. 6 and 8).

**Table 1**

The  $\text{NO}_x$  storage capacity of flame-made  $\text{BaCO}_3$  and  $\text{Pt}/\text{BaCO}_3$  in  $10^{-5} \text{ mol}_{\text{NO}_x} \text{ g}_{\text{cat}}^{-1}$  (A) and the ratio of the maximal possible storage amount calculated for  $\text{BaCO}_3$  (B).

Feed	100 °C $\text{BaCO}_3$		100 °C $\text{Pt}/\text{BaCO}_3$		400 °C $\text{BaCO}_3$		400 °C $\text{Pt}/\text{BaCO}_3$	
	A	B	A	B	A	B	A	B
NO	<1	<0.1%	<1	<0.1%	1	0.1%	1	0.1%
$\text{NO}/\text{O}_2$	1	0.1%	2	0.2%	4	0.4%	53	5.2%
$\text{NO}_2$	19	1.9%	20	2%	35	3.5%	93	9.2%

The  $\text{NO}_x$  adsorption on NSR catalyst compounds such as  $\text{BaCO}_3$  is an activated process so temperatures above ca. 100 °C are necessary to store  $\text{NO}_x$  in a reasonable time. This is shown by the temperature dependence of the  $\text{NO}_x$  storage rate. Therefore, the NSC should increase with temperature as long as no  $\text{NO}_x$  desorption occurs by nitrite or nitrate decomposition. Especially for Pt-containing  $\text{BaCO}_3$ , the parallel temperature-depending equilibrium reaction



has to be considered. The equilibrium shifts to the right-hand side of Eq. (2) for higher temperatures [35] and the changed NO/ $\text{NO}_2$  ratio with increasing NO concentration reduces the NSC as seen in Table 1 (compare feed variation experiments).

The influence of temperature was investigated by an experiment, shown in Fig. 10.  $\text{Pt}/\text{BaCO}_3$  was treated with  $\text{NO}_2$  for a certain time period. However, the sample was still far away from the maximum NSC. Starting from this condition the temperature was varied. During this experiment a constant  $\text{NO}_2$  feed was used and the gas composition at the reactor outlet was monitored. At 200 °C the feed remained in the form of  $\text{NO}_2$  (conversion rate to NO is only 3.5%) but the thermal activation was too low for fast  $\text{NO}_x$  storage. The conversion to NO increased to 26% after heating to 300 °C. At this temperature the thermal activation was high enough to facilitate fast  $\text{NO}_x$  storage and the  $\text{NO}_x$  breakthrough curve dropped down. This effect was reversible. Heating up to 400 °C led to a strong increase of the  $\text{NO}_x$  in the outlet and therefore less  $\text{NO}_x$  was stored. The low storage rate is attributed to the high  $\text{NO}_2$  conversion to NO which is approx. at 75%. Very small temperature changes around 400 °C affected the  $\text{NO}_2$  conversion remarkably which could easily rise up to 90%. An additional effect confirming the lower  $\text{NO}_x$  storage capacity is the slight thermal decomposition of stored nitrates starting at temperatures above 300 °C. Subsequent cooling down to 300 °C led again to more efficient  $\text{NO}_x$  storage.

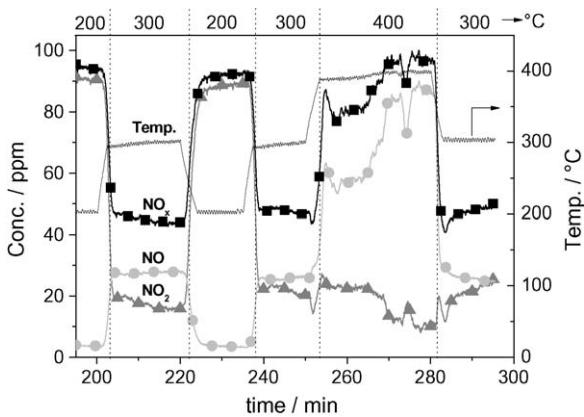
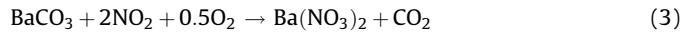


Fig. 10. Outlet gas composition during  $\text{NO}_2$  storage on  $\text{Pt}/\text{BaCO}_3$  at different temperatures.

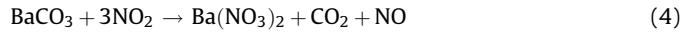
The results indicate the benefit of a careful control of the adsorption temperature for optimal working conditions (e.g. for technical application as NSR catalyst).

### 3.6. Adsorption versus solid state conversion

To form  $\text{Ba}(\text{NO}_3)_2$  from  $\text{BaCO}_3$ ,  $\text{NO}_2$  and  $\text{O}_2$  are required according to the overall reaction [36]:



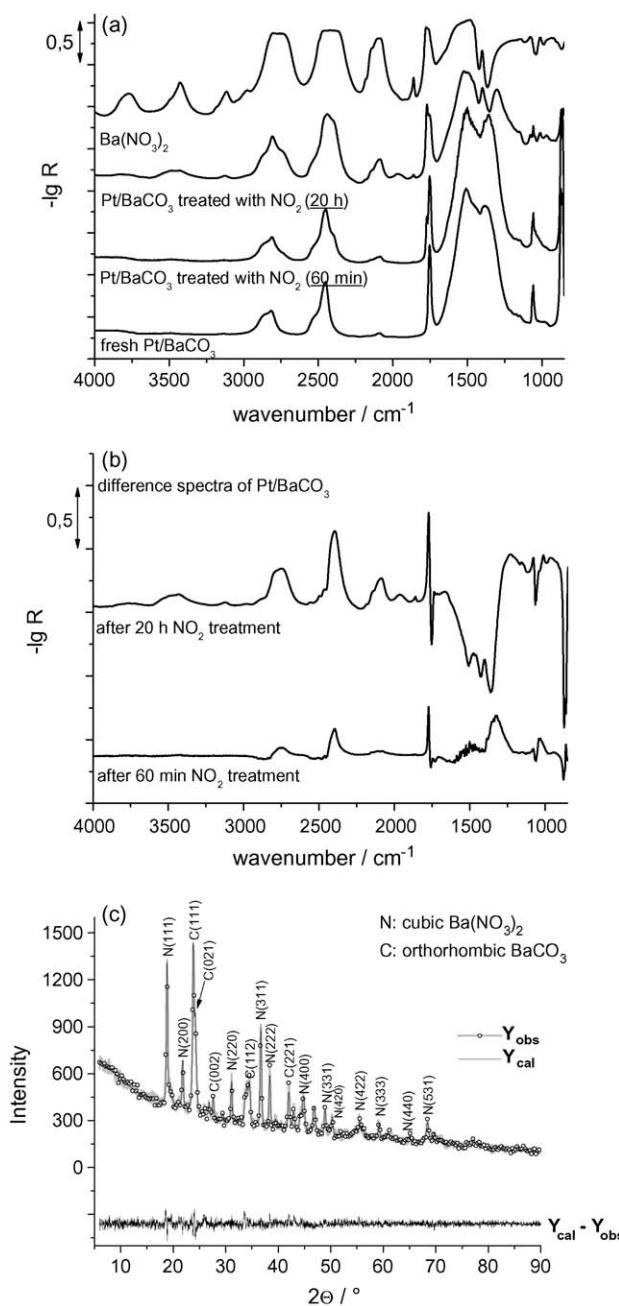
or  $\text{Ba}(\text{NO}_3)_2$  forms according to the modified Eq. (1), where NO and  $\text{CO}_2$  gases are released.



To investigate the sample with regard to barium nitrate formation,  $\text{Pt}/\text{BaCO}_3$  was treated with  $\text{NO}_2$  during a short (approx. 60 min) and a long run (approx. 20 h - until the  $\text{NO}_x$  inlet and outlet were equal) at 400 °C. Ex situ DRIFT spectra from these two experiments are presented in Fig. 11a. The solid state spectrum after 60 min of  $\text{NO}_2$  treatment indicates only a marginal change compared to the spectrum of fresh  $\text{Pt}/\text{BaCO}_3$ . The difference between these two spectra is shown in Fig. 11b (bottom) where bands of adsorbed nitrates can be observed (cf. Fig. 8). XRD patterns of this sample confirm that nearly the whole  $\text{NO}_2$ -treated sample remained as  $\text{BaCO}_3$ . Thus, formation of a significant amount of bulk nitrates could not be formed in the time period chosen.

In contrast, the DRIFT solid state spectrum of  $\text{Pt}/\text{BaCO}_3$  after 20 h of  $\text{NO}_2$  treatment shows more similarities to the spectrum of pure  $\text{Ba}(\text{NO}_3)_2$  (Fig. 11a). However, this solid state spectrum does not equal neither the spectra of pure  $\text{Ba}(\text{NO}_3)_2$  nor  $\text{Pt}/\text{BaCO}_3$ . The resulting difference after 20 h  $\text{NO}_2$  treatment can be seen in Fig. 11b (top). When comparing these two difference spectra in Fig. 11b, a different band structure becomes apparent in the spectrum obtained after longer  $\text{NO}_2$  treatment. This new band structure is probably caused by conversion of a part of bulk  $\text{BaCO}_3$  [37] into  $\text{Ba}(\text{NO}_3)_2$ . The XRD pattern of this sample (see Fig. 11c) confirms the assumption of two phases. In addition to the orthorhombic  $\text{BaCO}_3$  phase [31], a cubic  $\text{Ba}(\text{NO}_3)_2$  phase [38] was formed. In spite of the relatively long storage time (20 h), conversion was not complete (the obtained sample consists of 55 vol.% of carbonate and 45 vol.% of nitrate according to the Rietveld method [26,27]). Thus the chosen reaction time was too short for a complete carbonate conversion although the  $\text{NO}_x$  inlet and outlet were equal and therefore saturation was assumed. As a consequence of the increasing molar volume of a storage particle during  $\text{Ba}(\text{NO}_3)_2$  formation, small pores may cause a hindered diffusion into the core of the particle [36]. This effect may result in a decreased storage rate with increasing time of  $\text{NO}_2$  treatment. At high temperatures  $\text{NO}/\text{O}_2$  treatment of  $\text{Pt}/\text{BaCO}_3$  led to the same nitrate phase but resulted in a different carbonate/nitrate ratio.

To sum up, after short  $\text{NO}/\text{O}_2$  or even  $\text{NO}_2$  treatment (up to 60 min) the orthorhombic  $\text{BaCO}_3$  phase (XRD) remained whereas DRIFT spectra clearly showed adsorbate bands. Only long  $\text{NO}_x$  treatment at high temperatures lead to a reorganisation of the solid state lattice and consequently to the formation of bulk nitrates.



**Fig. 11.** (a) Solid state DRIFT spectra of Ba(NO<sub>3</sub>)<sub>2</sub>, Pt/BaCO<sub>3</sub> treated with NO<sub>2</sub> for 20 h and for 1 h and fresh Pt/BaCO<sub>3</sub> at 400 °C (top to down). (b) Difference in solid state spectra of fresh Pt/BaCO<sub>3</sub> with NO<sub>2</sub>-treated Pt/BaCO<sub>3</sub> (top: after 20 h, bottom: after 60 min). (c) XRD pattern of Pt/BaCO<sub>3</sub> treated with NO<sub>2</sub> (20 h) with the according Rietveld analysis. Important hkl lines of Ba(NO<sub>3</sub>)<sub>2</sub> (abbr. N) and BaCO<sub>3</sub> (abbr. C) are signed.

This means that for technical application (e.g. as NSR-automotive catalysts) NO<sub>x</sub> adsorption on the surface and subsurface region is contributing mainly to the storage effect.

#### 4. Conclusions

Storage of NO<sub>x</sub> on flame-made high SSA BaCO<sub>3</sub> and Pt/BaCO<sub>3</sub> nanoparticles was studied by DRIFT spectroscopy. Adsorption of NO on BaCO<sub>3</sub> resulted in nitrites while commercially available low SSA BaCO<sub>3</sub> did not give rise to detectable bands. In contrast, NO<sub>2</sub> storage investigations on commercial and flame-made BaCO<sub>3</sub> showed the same adsorbed species though the latter showed more

intensive bands. The presence of oxygen did not measurably affect adsorption on these Pt-free BaCO<sub>3</sub>. NO<sub>2</sub> was stored best affording the highest NSC. DRIFT spectra suggest that during NO<sub>2</sub> treatment of BaCO<sub>3</sub> small amounts of NO were formed in situ, adsorbed on the surface and subsequently oxidised by excess NO<sub>2</sub>. Higher temperatures favoured the NO<sub>x</sub> storage process.

Addition of Pt to BaCO<sub>3</sub> changed the structure of the BaCO<sub>3</sub> and resulted in a SSA of 110 m<sup>2</sup> g<sup>-1</sup> for the fresh powder. This SSA decreased to 60 m<sup>2</sup> g<sup>-1</sup> after pre-conditioning of the powder at 400 °C. The Pt enhanced the NO<sub>x</sub> storage at higher temperatures. In the presence of oxygen during NO adsorption, Pt catalysed NO oxidation and thus afforded higher NSC by direct NO<sub>2</sub> storage. Subsequent oxidation of previously stored NO could be corroborated by DRIFTS. The same adducts were observed upon NO<sub>2</sub> treatment. The maximum NSC on Pt/BaCO<sub>3</sub> was about 1 mol<sub>NO<sub>x</sub></sub> m g<sub>cat</sub><sup>-1</sup> after more than 20 h of NO<sub>2</sub> treatment.

Considering the temperature dependent equilibrium of NO<sub>2</sub> and NO/O<sub>2</sub> as well as the need of thermal activation of NO<sub>x</sub> storage, an optimal storage temperature exists which warrants reasonably fast storage rate coupled with high NSC. This temperature is between 300 and 400 °C for Pt/BaCO<sub>3</sub>.

A few minutes of NO<sub>x</sub> treatment afforded predominantly NO<sub>x</sub> adsorbates on the surface. Significant bulk barium nitrate formation was only observed after long NO<sub>x</sub> treatment at high temperatures as could be observed on Pt/BaCO<sub>3</sub>. In the latter case the storage rate decreased most likely because of hindered diffusion.

The flame-made barium-containing nanopowders showed some potential for application in NSR catalysis. Due to their high surface area compared to the corresponding conventionally prepared powders, the NSC is increased, and the practical application of such nanopowders in washcoats of monoliths seems feasible.

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